Influence of mixing and cooling on aerosol formation and evolution in backward-facing step flow

Arkadiusz K. Kuczaj^{1,2} Markus Nordlund¹ Edo Frederix² Bernard J. Geurts^{2,3}

¹Philip Morris International Research & Development, Philip Morris Products S.A., Neuchâtel, Switzerland ²Multiscale Modeling and Simulation, J.M. Burgers Center, University of Twente, Enschede, The Netherlands ³Anisotropic Turbulence, Fluid Dynamics Laboratory, Eindhoven University of Technology, Eindhoven, The Netherlands

A.K. Kuczaj et al. (PMI R&D, UT)

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2 Governing equations









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Background

Goals

- controlled aerosol generation from oversaturated vapors
- understand formation and evolution of aerosols
- identify parameters which influence physical/chemical aerosol characteristics at given conditions
- develop numerical methods for prediction of aerosol behavior

Main challenges

- vapor: multi-species mixtures
- aerosol: small droplets at high density
- flow: unsteady and density-varying (large temperature gradients)



CFD approach

Flow modeling

- low-Mach number approach
- in-house code based on OpenFOAM[®]: numerics & parallelization
- collocated mesh with PISO pressure-velocity coupling

Aerosol modeling

- Euler-Euler approach (one-way coupling)
- homogeneous nucleation
- condenstation/evaporation
- coalescence



Aerosol modeling

Development approach

- aerosol formation: single-species¹ \implies multi-species²
- validation: pipe flow³ \implies backward-facing step
- accuracy: PISO extension, TVD schemes, space-time refinement^{4,5}

References

- 1 Efficient second-order time integration for single-species aerosol formation and evolution, C. Winkelmann, M. Nordlund, A.K. Kuczaj, S. Stolz, B.J. Geurts, International Journal for Numerical Methods in Fluids, 74 (5), 2014
- 2 Multispecies aerosol formation due to rapid cooling of alcohol mixtures, C. Winkelmann, A.K. Kuczaj, M. Nordlund, B.J. Geurts, submitted to JAS
- 3 Extension of compressible PISO algorithm to single-species aerosol formation and transport, E.M.A. Frederix, M. Stanic, A.K. Kuczaj, M. Nordlund, B.J. Geurts, to be submitted
- 4 Capturing aerosol droplet nucleation and condensation bursts using PISO and TVD schemes, E.M.A. Frederix, A.K. Kuczaj, M. Nordlund, B.J. Geurts, this conference
- 5 Solution-adaptive space-time refinement for multispecies aerosol formation, B.J. Geurts, E.M.A. Frederix, A.K. Kuczaj, M. Nordlund, this conference

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Multispecies flow dynamics

Navier-Stokes flow:

$$\partial_t \rho + \nabla \cdot (\rho \mathbf{u}) = 0$$

$$\partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) = -\nabla \rho + \nabla \cdot (\mu \tau)$$

$$c_p \partial_t (\rho T) + c_p \nabla \cdot (\rho T \mathbf{u}) = \nabla \cdot (k \nabla T) + \mu \tau (\nabla \mathbf{u}) + D_t \rho + S_h$$

$$\partial_t (\rho Y_i) + \nabla \cdot (\rho Y_i \mathbf{u}) = \nabla \cdot (\rho D_i \nabla Y_i) + S_i^{I \to \mathbf{v}}; i = 1, \dots, n$$

$$\partial_t (\rho Z_i) + \nabla \cdot (\rho Z_i \mathbf{u}) = -S_i^{I \to \mathbf{v}}$$

$$\partial_t N + \nabla \cdot (N \mathbf{u}) = S_N$$

Assumptions:

- Mass fractions in gas Y_i and liquid Z_i state: $\sum_{i=1}^{n} (Y_i + Z_i) = 1$
- Dalton law for partial pressures of ideal gas: $p = \sum_{i=1}^{n} p_i^{v}; p_i^{v} = \rho k T \frac{Y_i}{m_i}$ (m_i molecular mass of species)

Soret, Dufour effects and diffusion of liquid droplets excluded

Binary diffusion with Fick law and Fuller method to approximate diffusion constant D_i

Aerosol droplet density N with fixed mean log-normal distribution

Aerosol formation and evolution

Multispecies aerosol dynamics

 Heat flow rate due to phase change ^(I→v) related to heat of evaporation:

 $S_h = -\sum_{i=1}^n \Delta h_i^{vap} S_i^{l \to v}$

• Liquid-vapor mass transfer due to nucleation, evaporation and condensation:

 $S_i^{l \to v} = -S_i^{nuc} + S_i^{e-c}$

• Rate of change of droplet density number due to nucleation, coalescence and evaporation:

 $S_N = J_N - J_c - J_{ev}$



Homogeneous nucleation

Classical nucleation theory

- Nucleation mass flow rate based on nucleation rate J_N of molecules number N_i with mass twice that of the critical cluster: $S_i^{nuc} = 2J_N N_i m_i$
- Nucleation rate $J_N = R_{av}Zc_{eq}$: average growth rate \times Zeldovich factor \times equilibrium concentration
- Average growth rate R_{av} based on the condensation rate (Ref. [1]) extended for multispecies mixture
- Zeldovich factor Z characterizes contribution of Brownian motion to the formation of critical cluster (Ref. [1])
- Equilibrium concentration of critical cluster (related to Gibbs free energy barrier to form an interface at the boundaries of a new phase) takes into account 'self-consistent' normalization (Ref. [2])

References:

- 1 H. Arstila, P. Korhonen, M. Kulmala, Ternary nucleation: kinetics and application to water-ammonia-hydrochloric acid system, Journal of Aerosol Science, 30, 1999
- 2 G. Wilemski, B. Wyslouzil, Binary nucleation kinetics, I. Self-consistent size distribution, J. Chem. Phys. 103, 1995

Condensation-evaporation

Mass flow rate due to evaporation/condensation S_i^{e-c}

- Separate treatment for each component (Ref. [1]): $S_i^{e-c} = 2\pi D_i \overline{d} \rho Y_i^s f(\overline{d}, \lambda) \left(E_i - \frac{S_i}{W_i} \right) N$
- $f(\overline{d}, \lambda)$ Fuchs factor (Knudsen correction) (Ref. [2])
- \overline{d} count mean diameter computed from diameter of average mass through Hatch-Choate conversion equation (Ref. [2])
- E_i equilibrium saturation takes into account Kelvin effect (Ref. [3])
- *S_i*, *W_i* saturation of species and mole fraction in the liquid phase (Raoult's law used)

References:

- 1 S. Friedlander, Smoke, Dust and Haze, Wiley, New York, 1977
- 2 W. Hinds, Aerosol Technology, Wiley-Interscience, New York, 1999
- 3 M. Wilck, F. Stratmann, A 2-D multicomponent modal aerosol model and its application to laminar flow reactors, Journal of Aerosol Science, 28, 1997

Rate of change of droplet density number $S_N = J_N - J_c - J_{ev}$

Coalescence rate J_c

- Binary collision mechanism: $J_c = \overline{K}N^2$
- Proportionality coefficient K based on the theory for polydisperse aerosols (Ref. [1])

Evaporation rate J_{ev}

- Complete droplets evaporation based on the consideration of mass balance
- Critical droplet diameter is computed
- Based on log-normal distribution, the droplets with size smaller than critical diameter are eliminated

References:

 K. Lee, H. Chen, Coagulation rate for polydisperse particles, Aerosol Science and Technology, 3, 1984

Single-species aerosol model validation

Laminar flow diffusion chamber (LFDC)

A.K

see: Capturing aerosol droplet nucleation and condensation bursts using PISO and TVD schemes, E.M.A. Frederix, A.K. Kuczaj, M. Nordlund, B.J. Geurts

U - velocity		
T - temperature		
Y - gas		
Z - liquid		
N - particle/droplet number density		
nucleation		
coagulation		
mass source term	_	
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Backward-facing step flow

Motivaton

- Canonical flow case
- Wide range of application: laminar-transition-turbulent
- More complex flow than in laminar flow diffusion chamber
- Shear layer mixing layer: various ways to utilize
- Mixing (geometry, Re) and cooling (wall temperature) can be studied

Flow behavior



T.P. Chiang, T.W.H. Sheu, C.C. Fang, Numerical investigation of vortical evolution in a backward-facing step expansion flow, Applied Mathematical Modeling, 23, 1999

B.F. Armaly, F. Durst, J.C.F. Pereira, B. Schoenung, Experimental and theoretical investigation of backward-facing step, J. Fluid Mech., 127, 1983



Backward-facing step



- Domain length based on the highest computed Re $(4 \times x_1)$
- Vapor mixture at saturated conditions at inlet
- Cooling wall T_w set constant
- Step-wall and upper wall with adiabatic conditions
- Laminar flow profile at the inlet



Flow - Re = 100 (top), 500, 1000, 1500 (bottom)

Velocity magnitude: $|\mathbf{u}|/U_m$



Vertical velocity: u_z/U_m





Temperature and vapor mass fraction

Temperature: $T/(T_m - T_w)$



Vapor mass fraction: Y/Y_0





Liquid mass fraction and droplet density number

Liquid mass fraction: Z/Y_0



Droplet density number: N





Nucleation and condensation/evaporation rate

Droplet nucleation rate

$Condensation/evaporation\ rate$





Quantification - example



Droplet number density profile at x = 6h

Mass fraction of gas species profile at x = 6h





Summary

- Multispecies aerosol model in Euler-Euler framework developed
- Backward-facing step adopted for study of aerosol formation and evolution
- Quantification of aerosol formation and evolution possible (droplet number density, droplet size, amount of vapors turned into liquid droplets
- Future: Extensive parameter study for benchmarking the system at various conditions

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